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Removal and recovery of ammonium and phosphate from wastewater by means of geopolymer-based adsorbents

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ENVIRONMENTAL, AND
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WHY PHOSPHATE RECOVERY BY ADSORPTION?

- Production of P-based fertilizers is expected to increase by 100% by 2050.
- P represents a limited resource. Unless a marked P recovery is implemented worldwide, **the peak of phosphate rock extraction is expected to be reached by 2040-50**
- Several technologies for phosphate recovery from municipal wastewater (MWW) are under development or optimization. They generally implement P recovery in the sludge line of wastewater treatment plants.
- **Adsorption** is not yet applied at full scale for P recovery, **but it represents an interesting option for P recovery both from the sludge line and wastewater line.**



WHY AMMONIUM RECOVERY BY ADSORPTION?

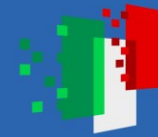
- Production of N-based fertilizers is expected to increase by 50% by 2050, starting from the current level of 110 million t/year.
- N is not a limited resource, but **ammonia production from atmospheric N₂ is a very energy-intensive process** (about 8000 kWh / t of NH₃ produced)
- In addition, **the traditional biological process for NH₄⁺ removal from MWW is energy intensive** (3300-3500 kWh / t NH₄⁺ removed) and does not allow any N recovery
- **NH₄⁺ recovery from MWW by adsorption, followed by the production of N-based fertilizers, represents an attractive option**, capable to drastically cut the energy requirement for both NH₄⁺ removal from MWW and N-based fertilizers production



THE GOAL OF THIS RESEARCH IS ...

... to develop and validate with real wastewater:

- **Innovative geopolymers for the removal of ammonium by cation exchange** from MWW and from effluents produced in the sludge treatment line
- **Innovative geopolymer / hydrotalcite composites for the contemporary removal of ammonium (by cation exchange) and phosphate (by adsorption / anion exchange)** from MWW and from effluents produced in the sludge treatment line



TESTED SORBENTS

Pure geopolymers
for NH_4^+ removal:

- K-G2: K-based geopolymer with Si:Al ratio = 2
- Na-G1.2: Na-based geopolymer with Si:Al ratio = 1.2

Pure hydrotalcites for
 PO_4^{3-} removal:

- S911 → Sorbacid 911: $[\text{Mg}_2\text{Al}_3(\text{OH})_2(2+x)]\text{CO}_3 \cdot n\text{H}_2\text{O}$
- P61 → Pural 61: 61% MgO, 39% Al_2O_3
- P70 → Pural 70: 70% MgO, 30% Al_2O_3
- P50 → Pural 50: 50% MgO, 50% Al_2O_3

**Geopolymer /
hydrotalcite
composites for
contemporary NH_4^+
& PO_4^{3-} removal:**

- K-G2 90% - S911 10%
- K-G2 90% - P61 10%
- K-G2 65% - P70 35%



All tests were conducted with the 2 types of **ACTUAL WASTEWATER**:

	WWTP effluent → N&P removal from the wastewater line	Sludge WW from centrifugation of digested municipal sludge → N&P removal from the sludge line
TSS (mg/L)	5.3 ± 0.6	0.3 ± 0.1
NH ₄ -N (mg/L)	40 ± 3	810 ± 21
PO ₄ ³⁻ -P (mg/L)	7 ± 1	122 ± 12
Na ⁺ (mg/L)	48 ± 3	120 ± 7
K ⁺ (mg/L)	11 ± 1	230 ± 4
Mg ²⁺ (mg/L)	21 ± 2	3.4 ± 0.5
Ca ²⁺ (mg/L)	14 ± 1	39 ± 1
Cl ⁻ (mg/L)	128 ± 15	221 ± 3
NO ³⁻ (mg/L)	0.81 ± 0.02	9.6 ± 0.2
SO ₄ ²⁻ (mg/L)	93 ± 6	14 ± 2
pH	7.6 ± 0.2	6.6 ± 0.4

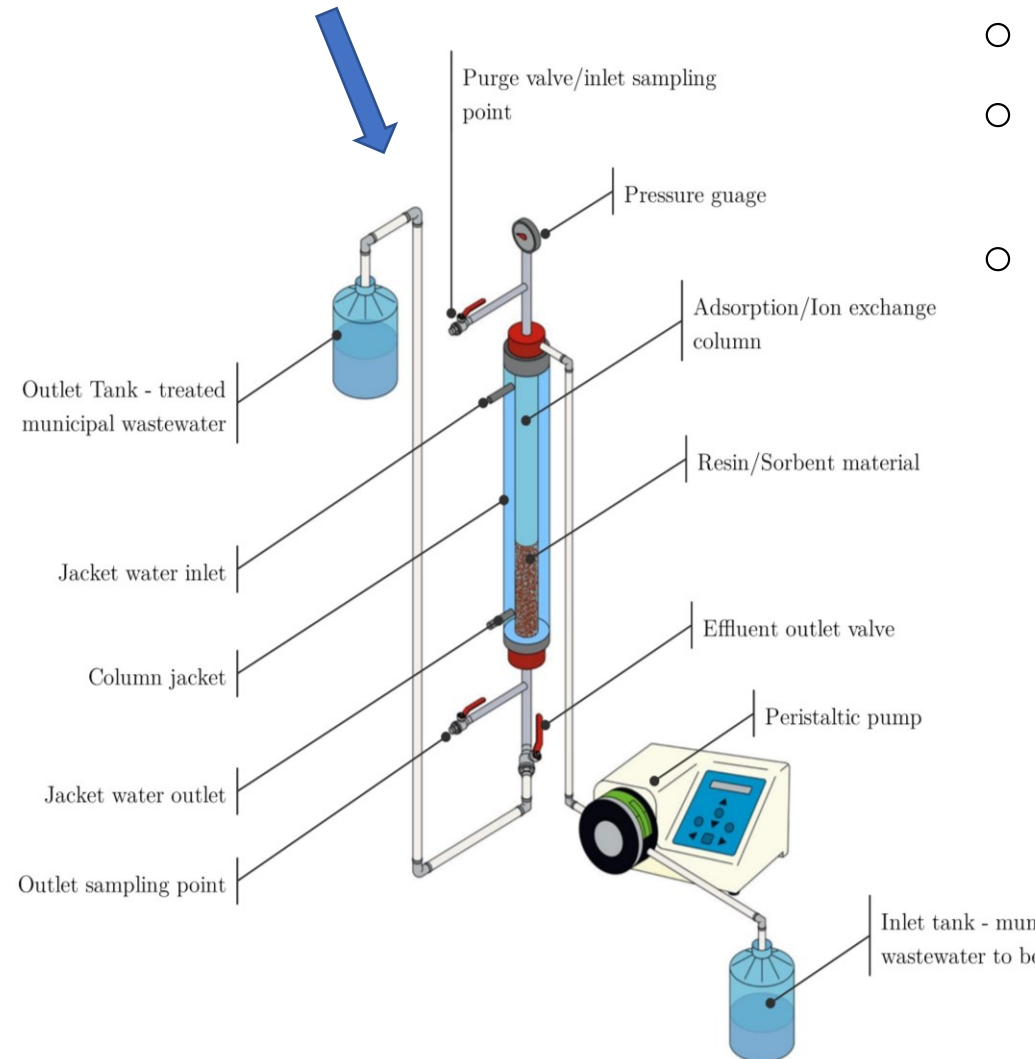
The tested WWs were pre-treated by microfiltration at 1 μm to avoid clogging of the packed adsorption columns



BATCH AND CONTINUOUS FLOW TESTS SETUP



- 125 mL borosilicate glass bottles
- Sorbent concentration: 2-5 g_{dry} sorbent/L
- Operating parameters:
 - orbital shaker 160 RPM
 - Temperature 22°C
 - Equilibrium time 24 h



- Resin bed height: 20-30 cm
- Empty bed contact time: 10-20 min
- Temperature: 22°C





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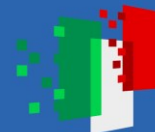


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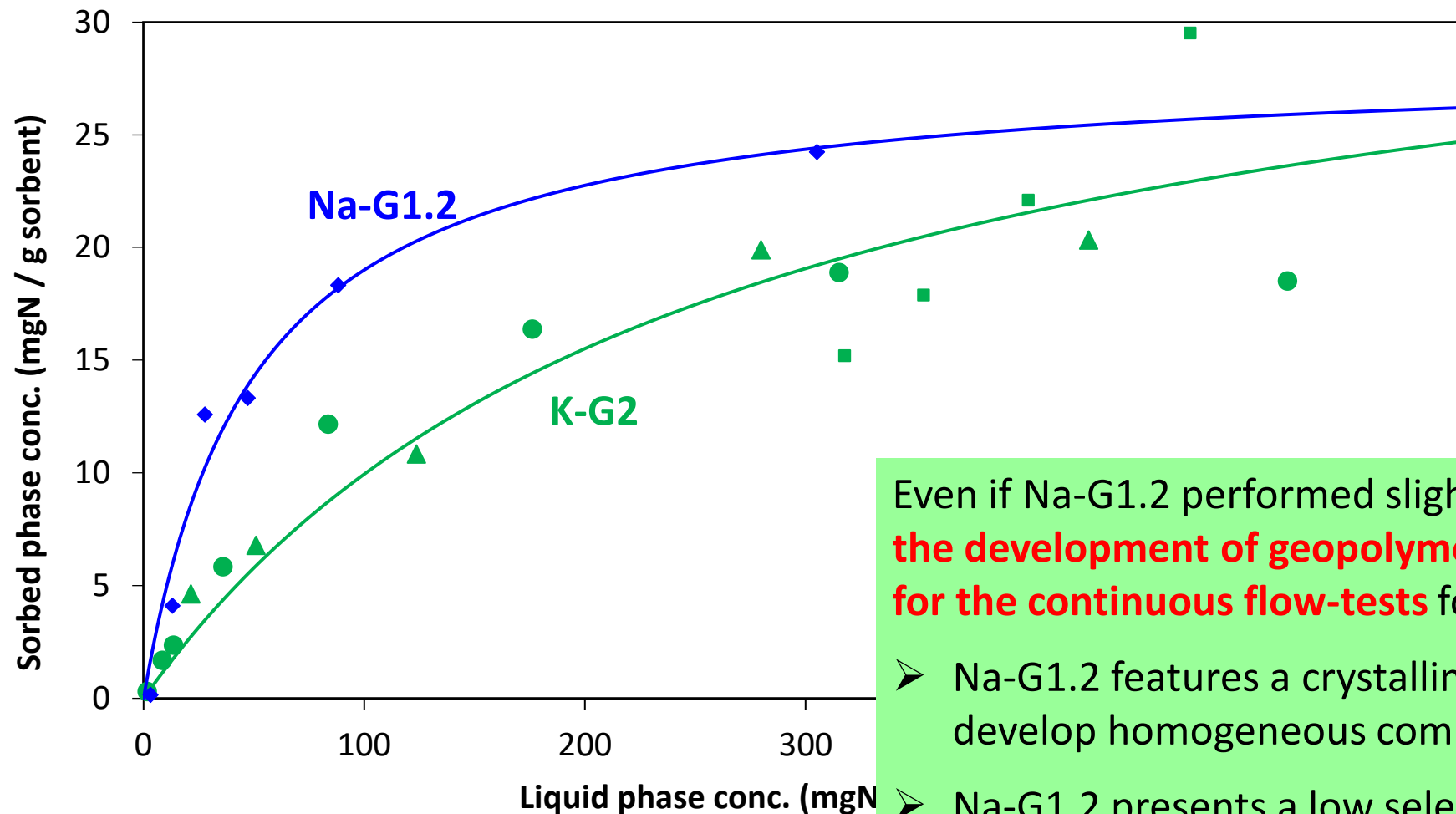


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1) AMMONIUM REMOVAL WITH PURE GEOPOLYMERS



AMMONIUM REMOVAL WITH PURE GEOPOLYMERS: BATCH ISOTHERMS



- Tests were conducted with sludge WW
- Experimental data + best-fitting Langmuir interpolation:

$$C_{S,eq} = \frac{C_{S_i}^{\infty} \cdot C_{L,eq}}{\frac{1}{K_{eq}} + C_{L,eq}}$$

Even if Na-G1.2 performed slightly better, **K-G2 was selected for the development of geopolymer / hydrotalcite composites and for the continuous flow-tests** for several reasons:

- Na-G1.2 features a crystalline phase that makes it difficult to develop homogeneous composites
- Na-G1.2 presents a low selectivity for ammonium in comparison to the other cations



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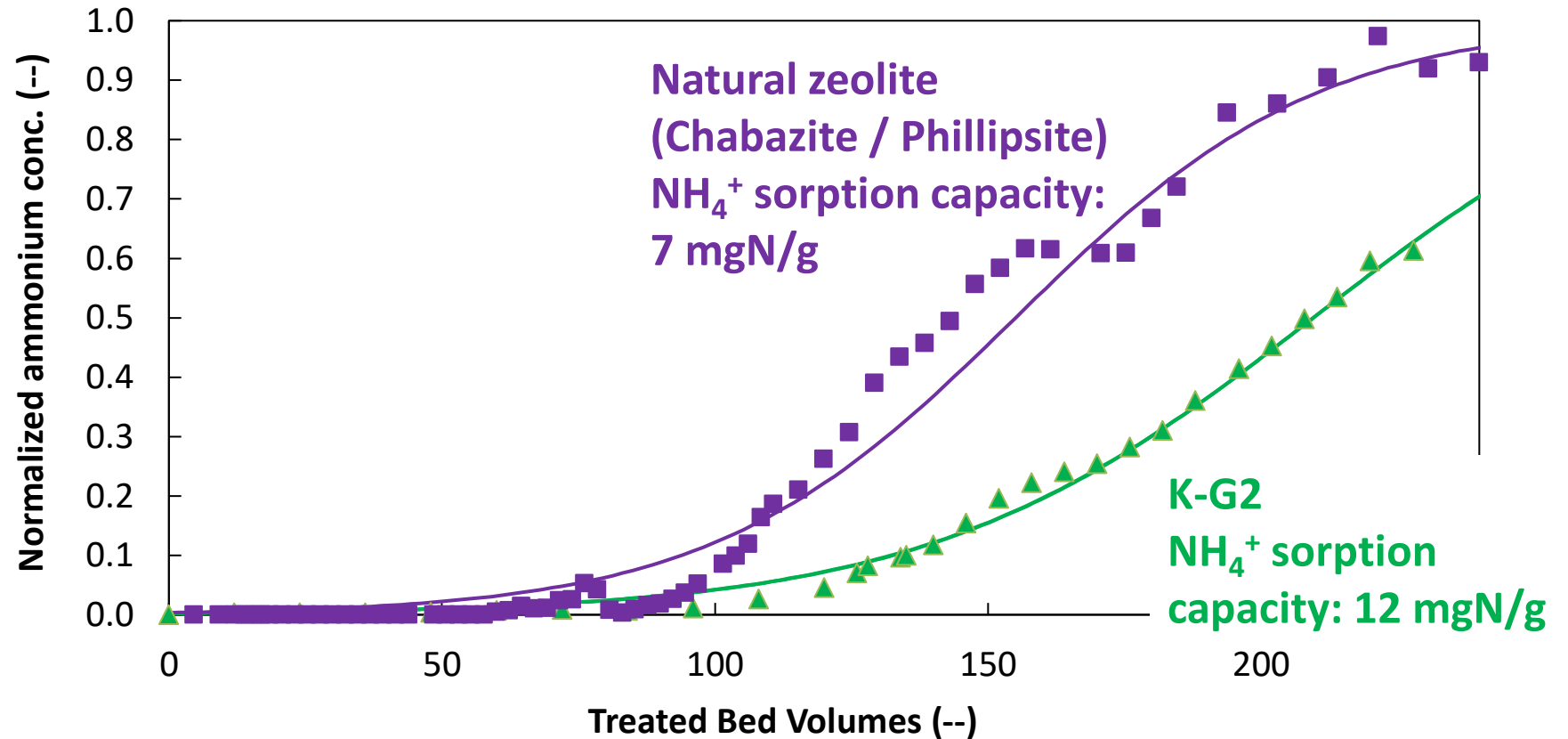
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AMMONIUM REMOVAL WITH GEOPOLYMER K-G2: CONTINUOUS FLOW TESTS

a) **Geopolymer K-G2** compared to a natural zeolite, tests conducted with WWTP effluent (40 mgN/L)

- Empty Bed Contact Time (EBCT): 10 min
- Resin bed height: 20-30 cm





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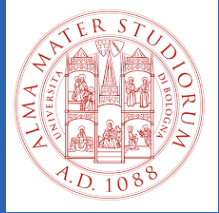


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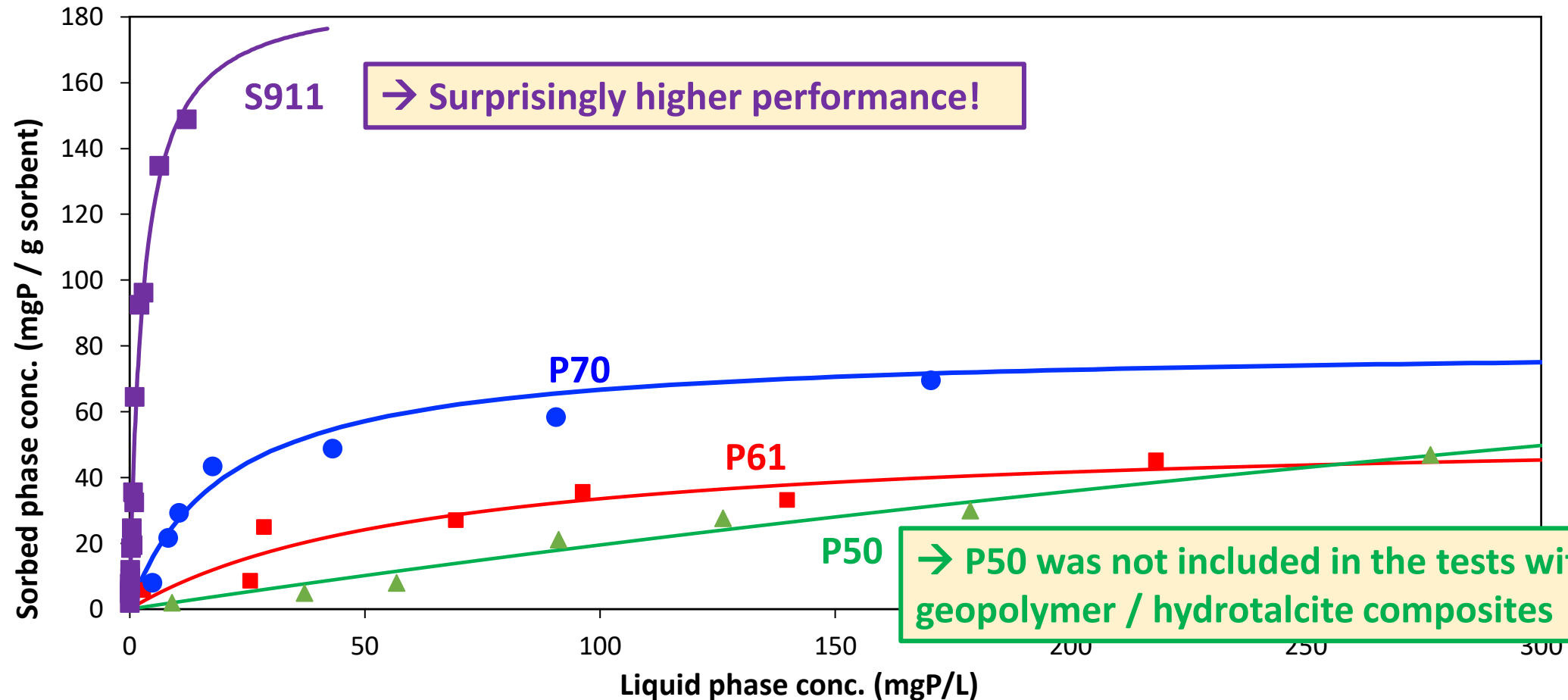


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2) SIMULTANEOUS AMMONIUM & PHOSPHATE REMOVAL WITH GEOPOLYMER / HYDROTALCITE COMPOSITES



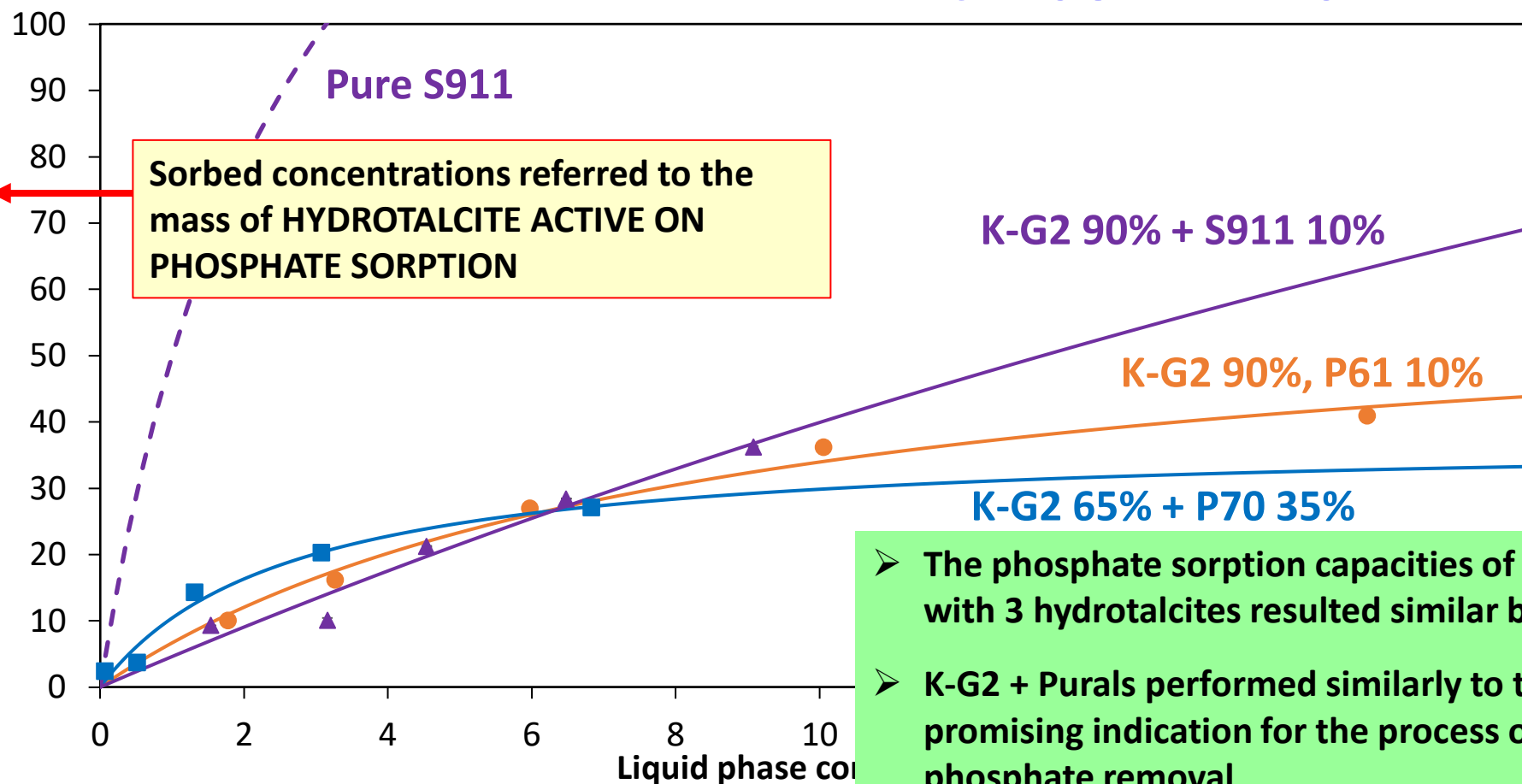
PHOSPHATE REMOVAL WITH GEOPOLYMER / HYDROTALCITE COMPOSITES: BATCH ISOTHERMS FOR THE PRELIMINARY SCREENING OF DIFFERENT HYDROTALCITES



PHOSPHATE REMOVAL WITH GEOPOLYMER / HYDROTALCITE COMPOSITES: BATCH ISOTHERMS

Sorbed phase P concentrations in equilibrium with 7 mgP/L in the liquid phase (mgP/g):

K-G2 + 35% P70	27
K-G2 + 10% S911	29
K-G2 + 10% P61	28
Pure P70	21
Pure S911	120 !



- The phosphate sorption capacities of the composites of geopolymer with 3 hydrotalcites resulted similar between each other
- K-G2 + Purals performed similarly to the corresponding pure Purals → promising indication for the process of contemporary ammonium & phosphate removal
- K-G2 + S911 performed worse than pure S911

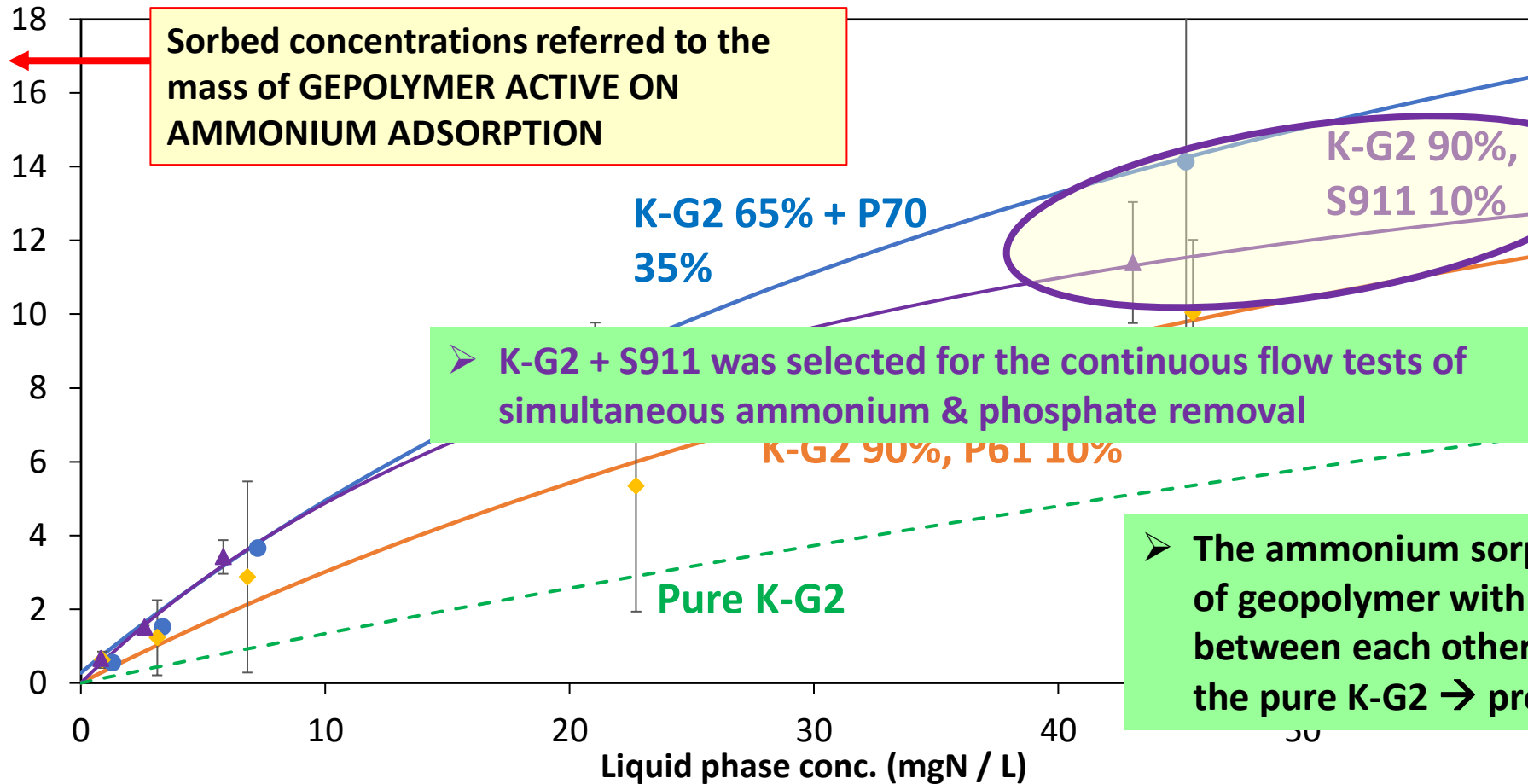
Sorbed phase conc. (mgP / g hydrotalcite active phase)

Liquid phase concentration



AMMONIUM REMOVAL WITH GEOPOLYMER / HYDROTALCITE COMPOSITES: BATCH ISOTHERMS

Sorbed phase conc. (mgN / g geopolimer active phase)



Sorbed phase NH_4^+ concentrations in equilibrium with 40 mgN/L in the liquid phase (mgN/g):

K-G2 + 35% P70	13
K-G2 + 10% S911	11
K-G2 + 10% P61	9
Pure K-G2	5

➤ The ammonium sorption capacities of the composites of geopolimer with 3 hydrothermalcites resulted similar between each other, and slightly higher than that of the pure K-G2 → promising indication!



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CONTINUOUS FLOW TESTS OF SIMULTANEOUS AMMONIUM & PHOSPHATE REMOVAL WITH THE K-G2 + S911 COMPOSITE...

... IN PROGRESS!



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CONCLUSIONS

- **The K-based geopolymer resulted a promising material for ammonium removal & recovery from both MWW (40 mgN/L) and sludge WW (810 mgN/L),** on both batch and continuous flow tests
- **Composites formed by the K-based geopolymer and 3 hydrotalcites led to promising results in terms of simultaneous ammonium & phosphate removal in batch isotherms.** Sorption capacities for both N & P resulted comparable to those of the corresponding pure materials, except for the surprisingly high performance of Sorbacid 911 alone
- Further research is needed to optimize the continuous flow adsorption / desorption process of simultaneous ammonium and phosphate removal



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GEopolymer based Adsorbents

GEA - GEopolymer based Adsorbents for effective adsorption and selective separation of CO₂ and eutrophication pollutants

PRIN: PROGETTI DI RICERCA DI RILEVANTE INTERESSE NAZIONALE – Bando 2022

Prot. 20229THRM2

CUP B53D23015240006

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